

PROGRAM : NATIONAL DIPLOMA

ENGINEERING: MECHANICAL

SUBJECT : FLUID MECHANICS III

CODE : IMF313

DATE : SSA JUNE EXAMINATION

17 JULY 2019

DURATION : (SESSION 1) 08:00 – 11:00 (3 HRS)

WEIGHT : 60% OF FINAL MARK

TOTAL MARKS : 100 MARKS

Examiner : MR VT. HASHE **Moderator** : MR S. SIMELANE

INSTRUCTIONS:

1. PLEASE ANSWER ALL QUESTIONS NEATLY

- 2. SHOW ALL CALCULATIONS
- 3. ANSWERS WITHOUT UNITS WILL BE PENALIZED
- 4. NUMBER YOUR ANSWERS STRICTLY ACCORDING TO THE QUESTION

NUMBER OF PAGES : 7 (Including cover page and 4 pages of annexures)

QUESTION 1

Water at 1 atm and 20°C is transported in a 150 m long circular concrete duct at a rate of 0.35 m³/s. If the duct length is now doubled while the diameter remains constant at 300 mm and the total head loss is 20 m, determine the drop in the flow rate through the duct. Take the concrete rougness as 1.2 mm. Only use Moody chart.

[20]

QUESTION 2

A 600 m long and 1 m diameter pipe is fitted with a ball valve at the outlet and leads from large water plastic tank. The pipe discharges to the atmosphere and the piezometric head at the inlet end of the pipe is 23 m relative to the outlet level. The head loss through the open ball valve is 10 times the velocity head in the pipe, other minor losses amount to twice the velocity head. If the Darcy friction factor has to be taken as constant at 0.02, estimate the fluid velocity after 12 seconds.

[20]

QUESTION 3

A cylindrical tank 0.9 m diameter is emptied through a 50 mm diameter pipe 3.6 m long (both ends being sharp) for which the friction factor is 0.04. Find the time taken for the fluid level to fall from 2.4 to 1.2 m over the outlet.

[20]

QUESTION 4

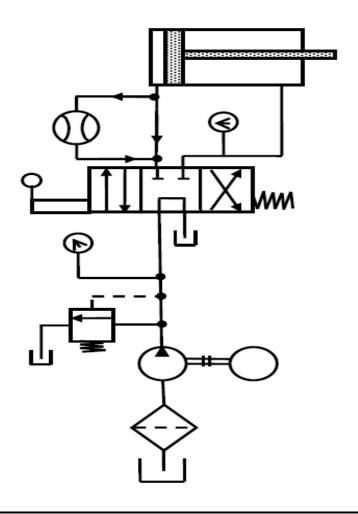
A junior engineer is tasked to investigate what happens if a firehose diameter of 60 mm and hose ending nozzle of 20 mm is increased to the diameter of 80 mm and a nozzle of 25 mm. The supply water pressure is maintained at 700 kPa inside the pipe and investigations show that a fireman is currently experiencing a force of 1.6 kN. Do the necessary investigations and briefly report on your finding

[21]

QUESTION 5

Figure 1 shows a circuit diagram for a particular application.

- (a) Redraw the circuit and identify the main components (8)
- (b) State the type of circuit and (1)
- (c) Explain how this circuit functions. (10)



[19]

$$Re = \frac{VD}{\nu}$$

$$V = \frac{\dot{V}}{A_c}$$

$$h_L = f \frac{L}{D} \frac{V^2}{2g}$$

$$h_L = K_L \frac{V^2}{2g}$$

 $F = \dot{m}v$

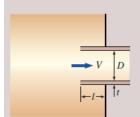
TABLE A-9							
Propertie Temp. <i>T</i> , °C	Density ρ , kg/m ³	Specific Heat c_p J/kg·K	Thermal Conductivity k, W/m·K	Thermal Diffusivity α , m ² /s	Dynamic Viscosity μ, kg/m·s	Kinematic Viscosity ν, m ² /s	Prandtl Number Pr
-150 -100 -50 -40 -30	2.866 2.038 1.582 1.514 1.451	983 966 999 1002 1004	0.01171 0.01582 0.01979 0.02057 0.02134	4.158 × 10 ⁻⁶ 8.036 × 10 ⁻⁶ 1.252 × 10 ⁻⁵ 1.356 × 10 ⁻⁵ 1.465 × 10 ⁻⁵	8.636 × 10 ⁻⁶ 1.189 × 10 ⁻⁶ 1.474 × 10 ⁻⁵ 1.527 × 10 ⁻⁵ 1.579 × 10 ⁻⁵	3.013 × 10 ⁻⁶ 5.837 × 10 ⁻⁶ 9.319 × 10 ⁻⁶ 1.008 × 10 ⁻⁵ 1.087 × 10 ⁻⁵	0.7246 0.7263 0.7440 0.7436 0.7425
-20 -10 0 5	1.394 1.341 1.292 1.269 1.246	1005 1006 1006 1006 1006	0.02211 0.02288 0.02364 0.02401 0.02439	1.578×10^{-5} 1.696×10^{-5} 1.818×10^{-5} 1.880×10^{-5} 1.944×10^{-5}	$\begin{array}{c} 1.630 \times 10^{-5} \\ 1.680 \times 10^{-5} \\ 1.729 \times 10^{-5} \\ 1.754 \times 10^{-5} \\ 1.778 \times 10^{-5} \end{array}$	$\begin{array}{c} 1.169 \times 10^{-5} \\ 1.252 \times 10^{-5} \\ 1.338 \times 10^{-5} \\ 1.382 \times 10^{-5} \\ 1.426 \times 10^{-5} \end{array}$	0.7408 0.7387 0.7362 0.7350 0.7336
15 20 25 30 35	1.225 1.204 1.184 1.164 1.145	1007 1007 1007 1007 1007	0.02476 0.02514 0.02551 0.02588 0.02625	$\begin{array}{c} 2.009 \times 10^{-5} \\ 2.074 \times 10^{-5} \\ 2.141 \times 10^{-5} \\ 2.208 \times 10^{-5} \\ 2.277 \times 10^{-5} \end{array}$	$\begin{array}{c} 1.802\times10^{-5}\\ 1.825\times10^{-5}\\ 1.849\times10^{-5}\\ 1.872\times10^{-5}\\ 1.895\times10^{-5} \end{array}$	$\begin{array}{c} 1.470 \times 10^{-5} \\ 1.516 \times 10^{-5} \\ 1.562 \times 10^{-5} \\ 1.608 \times 10^{-5} \\ 1.655 \times 10^{-5} \end{array}$	0.7323 0.7309 0.7296 0.7282 0.7268
40 45 50 60 70	1.127 1.109 1.092 1.059 1.028	1007 1007 1007 1007 1007	0.02662 0.02699 0.02735 0.02808 0.02881	$\begin{array}{c} 2.346 \times 10^{-5} \\ 2.416 \times 10^{-5} \\ 2.487 \times 10^{-5} \\ 2.632 \times 10^{-5} \\ 2.780 \times 10^{-5} \end{array}$	$\begin{array}{c} 1.918 \times 10^{-5} \\ 1.941 \times 10^{-5} \\ 1.963 \times 10^{-5} \\ 2.008 \times 10^{-5} \\ 2.052 \times 10^{-5} \end{array}$	$\begin{array}{c} 1.702\times10^{-5}\\ 1.750\times10^{-5}\\ 1.798\times10^{-5}\\ 1.896\times10^{-5}\\ 1.995\times10^{-5} \end{array}$	0.7255 0.7241 0.7228 0.7202 0.7177

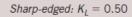
Loss coefficients K_L of various pipe components for turbulent flow (for use in the relation $h_L = K_L V^2/(2g)$, where V is the average velocity in the pipe that contains the component)*

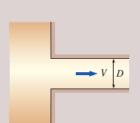
Pipe Inlet

Reentrant: $K_L = 0.80$

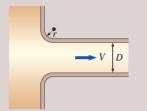
 $(t \ll D \text{ and } \bar{l} \approx 0.1D)$





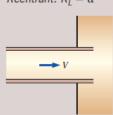


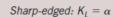
Well-rounded (r/D > 0.2): $K_L = 0.03$ Slightly rounded (r/D = 0.1): $K_L = 0.12$ (see Fig. 8-39)

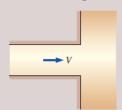


Pipe Exit

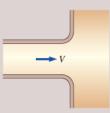
Reentrant: $K_L = \alpha$







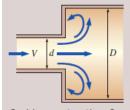
Rounded:
$$K_L = \alpha$$



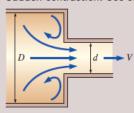
Note: The kinetic energy correction factor is $\alpha=2$ for fully developed laminar flow, and $\alpha\approx1.05$ for fully developed turbulent flow.

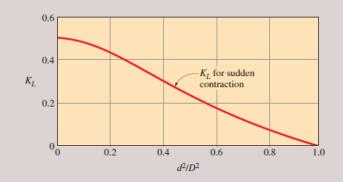
Sudden Expansion and Contraction (based on the velocity in the smaller-diameter pipe)

Sudden expansion: $K_L = \alpha \left(1 - \frac{d^2}{D^2}\right)^2$

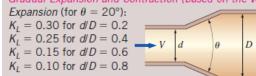


Sudden contraction: See chart.





Gradual Expansion and Contraction (based on the velocity in the smaller-diameter pipe)



Contraction:

$$K_L = 0.02 \text{ for } \theta = 30^{\circ}$$

 $K_L = 0.04 \text{ for } \theta = 45^{\circ}$
 $K_L = 0.07 \text{ for } \theta = 60^{\circ}$

$$K_L = 0.04 \text{ for } \theta = 45$$

 $K_L = 0.07 \text{ for } \theta = 60^\circ$

