

PROGRAM	: BENGTECH ENGINEERING: MECHANICAL
SUBJECT	: FLUID MECHANICS II
CODE	: FLMMIA2
DATE	: JUNE MAIN EXAMINATION 25 May 2019
DURATION	: (SESSION 1) 08:30 – 11:30 AM
WEIGHT	: 60% OF FINAL MARK
TOTAL MARKS	: 100 MARKS
Examiner	: MR VT. HASHE
Moderator	: MR S. SIMELANE

INSTRUCTIONS:

- 1. PLEASE ANSWER ALL QUESTIONS NEATLY
- 2. SHOW ALL CALCULATIONS
- 3. ANSWERS WITHOUT UNITS WILL BE PENALIZED
- 4. NUMBER YOUR ANSWERS STRICTLY ACCORDING TO THE QUESTIONS
- 5. DRAW DIADRAMS

NUMBER OF PAGES : 9 including cover page and 3 pages annexure

1.1 A thin 30 x 30 cm flat plate is pulled at 3 m/s horizontally through a 3.6 mm SAE 30 engine oil layer sandwiched between two plates, one stationary and the other moving at a constant velocity of 0.3 m/s. The dynamic viscosity of the oil is 0.027 Pa.s. Assuming the velocity in each oil layer to vary linearly (and indicating any two further assumptions used in arriving to the solution).

(a) Plot a detailed velocity profile and locate where the oil velocity is zero and (8)

- (b) Investigate if a force of 7.29 N will be sufficient to maintain the motion. (10)
- 1.2 The magnitude of the capillary rise in a circular tube can be determined from a force balance on the cylindrical liquid column of height *h* in the tube. With the use of a figure, prove that the capillary rise and depression are given by:

$$h = \frac{2\sigma}{\rho g R} \cos \phi$$

Use two separate schematic diagrams for both the rise and depression phenomena.

(15)

1.3 A pump is used to transport water at 20°C to a higher reservoir. If cavitation is to be avoided, what is the minimum pressure that must exist in the pump to avoid cavitation?
(2)

Figure 2 shows a differential manometer of U-tube type. Evaluate (showing all steps of your calculations) if the differential pressure is given by the expression:

$$P_A - P_B = gh(\rho_G - \rho_1) + \rho_2 gy - \rho_1 gx$$

Where ρ_G , ρ_1 and ρ_2 are the density of heavy liquid, density of liquid at A and density of liquid at B respectively. (7)

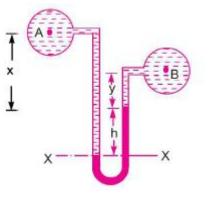


Figure 2



(4)

A vertical sluice gate is used to cover an opening and closing of the Vaal dam. The opening is 2 m wide and 1.2 m high as shown in Figure 3. On the upstream of the gate, the liquid of specific gravity 1.45 lies up to a height of 1.5 m above the top of the gate, whereas on the downstream side the water is available up to a height touching the top of the gate.

- a) Find the magnitude (Newtons) and the position (metres) of the resultant force
 - (28)
- b) Prove (using calculations) that a horizontal force of 9.597 kN acting at the top of the gate is capable of opening the gate.

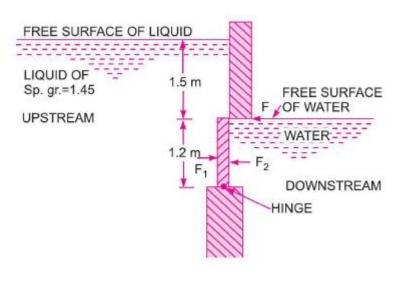
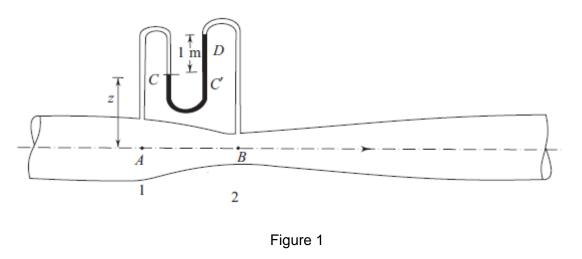


Figure 3

[32]

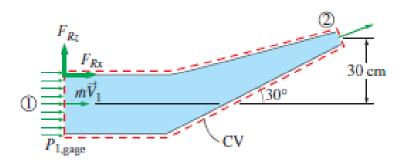
Develop an expression necessary to calculate the coefficient of discharge of a venturimeter shown in figure 4.



[10]

QUESTION 5

A reducing elbow in Figure 5 is used to deflect water flow from a fire engine truck to a burning building. Water is allowed to flow through the elbow at a rate of 14 kg/s in a horizontal pipe upward 30° while accelerating. The elbow discharges water into the atmosphere. The cross sectional area of the elbow is 113 cm² at the inlet and 7 cm² at the outlet. The elevation difference between the centres of the outlet and the inlet is 30 cm. Verify if an anchoring force of 144 N will be sufficient to hold the elbow in place.



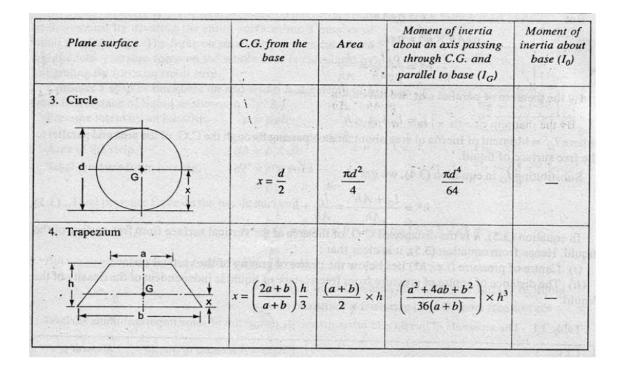
Proper	ties of satu	rated w	ater											
Temp. 7, °C	Saturation Pressure P _{sat} , kPa		nsity kg/m³ Vapor	Enthalpy of Vaporizatio <i>h</i> fg, kJ/kg	n ^c p	pecific Heat , J/kg-K Vapor	Condu	rmal uctivity Vm-K Vapor	Dynamic ' µ, kg Liquid		Prand Numb Pr Liquid		Volume Expansion Coefficient β, 1/K Liquid	Surface Tension, N/m Liquid
0.01 5 10 15 20	0.6113 0.8721 1.2276 1.7051 2.339	999.8 999.9 999.7 999.1 998.0	0.0048 0.0068 0.0094 0.0128 0.0173	2501 2490 2478 2466	4217 4205 4194 4186 4182	1854 1857 1862 1863 1867	0.561 0.571 0.580 0.589 0.598	0.0171 0.0173 0.0176 0.0179 0.0182	$\begin{array}{c} 1.792\times 10^{-3}\\ 1.519\times 10^{-3}\\ 1.307\times 10^{-3}\\ 1.138\times 10^{-3}\\ 1.002\times 10^{-3} \end{array}$	$\begin{array}{c} 0.922 \times 10^{-5} \\ 0.934 \times 10^{-5} \\ 0.946 \times 10^{-5} \\ 0.959 \times 10^{-5} \\ 0.973 \times 10^{-5} \end{array}$	11.2 9.45 8.09	1.00 1.00 1.00 1.00 1.00	$\begin{array}{c} -0.068\times 10^{-3}\\ 0.015\times 10^{-3}\\ 0.733\times 10^{-3}\\ 0.138\times 10^{-3}\\ 0.195\times 10^{-3}\end{array}$	0.0756 0.0749 0.0742 0.0735 0.0727
25 30 35 40 45	3.169 4.246 5.628 7.384 9.593	997.0 996.0 994.0 992.1 990.1	0.0231 0.0304 0.0397 0.0512 0.0655	2431 2419 2407	4180 4178 4178 4179 4180	1870 1875 1880 1885 1892	0.607 0.615 0.623 0.631 0.637	0.0186 0.0189 0.0192 0.0196 0.0200	$\begin{array}{c} 0.891\times 10^{-3}\\ 0.798\times 10^{-3}\\ 0.720\times 10^{-3}\\ 0.653\times 10^{-3}\\ 0.596\times 10^{-3} \end{array}$	$\begin{array}{c} 0.987 \times 10^{-5} \\ 1.001 \times 10^{-5} \\ 1.016 \times 10^{-5} \\ 1.031 \times 10^{-5} \\ 1.046 \times 10^{-5} \end{array}$	5.42 4.83 4.32	1.00 1.00 1.00 1.00 1.00	$\begin{array}{c} 0.247 \times 10^{-3} \\ 0.294 \times 10^{-3} \\ 0.337 \times 10^{-3} \\ 0.377 \times 10^{-3} \\ 0.415 \times 10^{-3} \end{array}$	0.0720 0.0712 0.0704 0.0696 0.0688
50 55 60 65 70	12.35 15.76 19.94 25.03 31.19	988.1 985.2 983.3 980.4 977.5	0.0831 0.1045 0.1304 0.1614 0.1983	2371 2359 2346	4181 4183 4185 4187 4190	1900 1908 1916 1926 1936	0.644 0.649 0.654 0.659 0.663	0.0204 0.0208 0.0212 0.0216 0.0221	$\begin{array}{c} 0.547 \times 10^{-3} \\ 0.504 \times 10^{-3} \\ 0.467 \times 10^{-3} \\ 0.433 \times 10^{-3} \\ 0.404 \times 10^{-3} \end{array}$	$\begin{array}{c} 1.062 \times 10^{-5} \\ 1.077 \times 10^{-5} \\ 1.093 \times 10^{-5} \\ 1.110 \times 10^{-5} \\ 1.126 \times 10^{-5} \end{array}$	2.99 2.75	1.00 1.00 1.00 1.00 1.00	$\begin{array}{c} 0.451 \times 10^{-3} \\ 0.484 \times 10^{-3} \\ 0.517 \times 10^{-3} \\ 0.548 \times 10^{-3} \\ 0.578 \times 10^{-3} \end{array}$	0.0679 0.0671 0.0662 0.0654 0.0645
75 80 85 90 95	38.58 47.39 57.83 70.14 84.55	974.7 971.8 968.1 965.3 961.5	0.2421 0.2935 0.3536 0.4235 0.5045	2309 2296 2283	4193 4197 4201 4206 4212	1948 1962 1977 1993 2010	0.667 0.670 0.673 0.675 0.677	0.0225 0.0230 0.0235 0.0240 0.0246	$\begin{array}{c} 0.378 \times 10^{-3} \\ 0.355 \times 10^{-3} \\ 0.333 \times 10^{-3} \\ 0.315 \times 10^{-3} \\ 0.297 \times 10^{-3} \end{array}$	$\begin{array}{c} 1.142 \times 10^{-5} \\ 1.159 \times 10^{-5} \\ 1.176 \times 10^{-5} \\ 1.193 \times 10^{-5} \\ 1.210 \times 10^{-5} \end{array}$	2.08 1.96	1.00 1.00 1.00 1.00 1.00	$\begin{array}{c} 0.607 \times 10^{-3} \\ 0.653 \times 10^{-3} \\ 0.670 \times 10^{-3} \\ 0.702 \times 10^{-3} \\ 0.716 \times 10^{-3} \end{array}$	0.0636 0.0627 0.0617 0.0608 0.0599
100 110 120 130 140	101.33 143.27 198.53 270.1 361.3	957.9 950.6 943.4 934.6 921.7	0.5978 0.8263 1.121 1.496 1.965		4217 4229 4244 4263 4286	2029 2071 2120 2177 2244	0.679 0.682 0.683 0.684 0.683	0.0251 0.0262 0.0275 0.0288 0.0301	$\begin{array}{c} 0.282 \times 10^{-3} \\ 0.255 \times 10^{-3} \\ 0.232 \times 10^{-3} \\ 0.213 \times 10^{-3} \\ 0.197 \times 10^{-3} \end{array}$	$\begin{array}{c} 1.227 \times 10^{-5} \\ 1.261 \times 10^{-5} \\ 1.296 \times 10^{-5} \\ 1.330 \times 10^{-5} \\ 1.365 \times 10^{-5} \end{array}$	1.58 1.44	1.00 1.00 1.00 1.01 1.02	$\begin{array}{c} 0.750 \times 10^{-3} \\ 0.798 \times 10^{-3} \\ 0.858 \times 10^{-3} \\ 0.913 \times 10^{-3} \\ 0.970 \times 10^{-3} \end{array}$	0.0589 0.0570 0.0550 0.0529 0.0509
150 160 170 180 190	475.8 617.8 791.7 1,002.1 1,254.4	916.6 907.4 897.7 887.3 876.4	2.546 3.256 4.119 5.153 6.388	2114 2083 2050 2015 1979	4311 4340 4370 4410 4460	2314 2420 2490 2590 2710	0.682 0.680 0.677 0.673 0.669	0.0316 0.0331 0.0347 0.0364 0.0382	$\begin{array}{c} 0.183 \times 10^{-3} \\ 0.170 \times 10^{-3} \\ 0.160 \times 10^{-3} \\ 0.150 \times 10^{-3} \\ 0.142 \times 10^{-3} \end{array}$	$\begin{array}{c} 1.399 \times 10^{-5} \\ 1.434 \times 10^{-5} \\ 1.468 \times 10^{-5} \\ 1.502 \times 10^{-5} \\ 1.537 \times 10^{-5} \end{array}$	1.09 1.03 0.983	1.02 1.05 1.05 1.07 1.09	$\begin{array}{c} 1.025\times10^{-3}\\ 1.145\times10^{-3}\\ 1.178\times10^{-3}\\ 1.210\times10^{-3}\\ 1.280\times10^{-3} \end{array}$	0.0487 0.0466 0.0444 0.0422 0.0399
200 220 240 260 280	1,553.8 2,318 3,344 4,688 6,412	864.3 840.3 813.7 783.7 750.8	7.852 11.60 16.73 23.69 33.15	1941 1859 1767 1663 1544	4500 4610 4760 4970 5280	2840 3110 3520 4070 4835	0.663 0.650 0.632 0.609 0.581	0.0401 0.0442 0.0487 0.0540 0.0605	$\begin{array}{c} 0.134\times 10^{-3}\\ 0.122\times 10^{-3}\\ 0.111\times 10^{-3}\\ 0.102\times 10^{-3}\\ 0.094\times 10^{-3} \end{array}$	$\begin{array}{c} 1.571 \times 10^{-5} \\ 1.641 \times 10^{-5} \\ 1.712 \times 10^{-5} \\ 1.788 \times 10^{-5} \\ 1.870 \times 10^{-5} \end{array}$	0.865 0.836 0.832	1.15 1.24 1.35	$\begin{array}{c} 1.350 \times 10^{-3} \\ 1.520 \times 10^{-3} \\ 1.720 \times 10^{-3} \\ 2.000 \times 10^{-3} \\ 2.380 \times 10^{-3} \end{array}$	0.0377 0.0331 0.0284 0.0237 0.0190
300 320 340 360 374.14	8,581 11,274 14,586 18,651 22,090	713.8 667.1 610.5 528.3 317.0	46.15 64.57 92.62 144.0 317.0	1405 1239 1028 720 0	5750 6540 8240 14,690 —	5980 7900 11,870 25,800 	0.548 0.509 0.469 0.427 	0.0695 0.0836 0.110 0.178 —	$\begin{array}{c} 0.086 \times 10^{-3} \\ 0.078 \times 10^{-3} \\ 0.070 \times 10^{-3} \\ 0.060 \times 10^{-3} \\ 0.043 \times 10^{-3} \end{array}$	$\begin{array}{c} 1.965 \times 10^{-5} \\ 2.084 \times 10^{-5} \\ 2.255 \times 10^{-5} \\ 2.571 \times 10^{-5} \\ 4.313 \times 10^{-5} \end{array}$	1.23	1.69 1.97 2.43 3.73	2.950 × 10− ³	0.0144 0.0099 0.0056 0.0019 0

Liquid	Density	Dynamic viscosity	Surface tension	Bulk modulus
	ρ	μ	σ	K
	[kg.m ⁻³]	[kg.m ⁻¹ s ⁻¹]	$[N.m^{-1}]$	$[GN.m^{-2}]$
Alcohol, ethyl	789	1.197 x10 ⁻³	0.0223	1.32
Benzene	879	0.647 x 10 ⁻³	0.0289	1.1
Carbon tetrachloride	1632	0.972 x 10 ⁻³	0.0268	1.12
Glycerol	1262	620 x 10 ⁻³	0.063	4.03
Mercury	13546	1.552 x 10 ⁻³	0.472	26.2
Paraffin oil	800	1.900 x 10 ⁻³	0.026	1.62
Water, sea	1025	$1.120 \ge 10^{-3}$	Assume sam	e as for tap water

PHYSICAL PROPERTIES OF COMMON LIQUIDS AT 20°C AND 1 ATMOSPHERE

Table 3.1 The moments of inertia and other geometric properties of some important plane surfaces

Plane surface	C.G. from the base	Area	Moment of inertia about an axis passing through C.G. and parallel to base (I _G)	Moment of inertia about base (I_0)	
1. Rectangle		atrus 10	and and a state of the state of	ala na tala quiqto atsiv aniq to diqu	
	$x = \frac{d}{2}$	bd	<u>bd</u> ³ 12	$\frac{bd^3}{3}$	
2. Triangle	10. 12.180	NY RE			
	$x = \frac{h}{3}$	<u>bh</u> 2	$\frac{bh^3}{36}$	$\frac{bh^3}{12}$	



FORMULAS

 $\mathbf{P} = \mathbf{F}/\mathbf{A}$

 $\tau = \mu du/dy$

 $h = 4\delta Cos \emptyset / \rho g d$

 $h = 4\delta/\rho g d$

p = ρgh

 $F = \rho g A \hbar$

 $\hat{\mathbf{h}} = (\mathbf{I}_{\mathbf{G}} \operatorname{Sin}^2 \emptyset / \mathbf{A} \hbar) + \hbar$

 $\hat{\mathbf{h}} = (\mathbf{I}_{G}/\mathbf{A}\hbar) + \hbar$

 $P/\rho + v^2/2g + z = c$

 $\dot{m} = \rho A v$