



**PROGRAM** : BACCALAUREUS TECHNOLGIAE  
*CHEMICAL ENGINEERING*

**SUBJECT** : UNIT OPERATIONS IV

**CODE** : WARB432

**DATE** : WINTER EXAMINATION

28 MAY 2016

**DURATION** : (SESSION 2) 12:30 - 15:30

**WEIGHT** : 40 : 60

**TOTAL MARKS** : 100

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**EXAMINER** : DR K MOOTHI

**MODERATOR** : PROF MS ONYANGO

**NUMBER OF PAGES** : 13 PAGES

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**INSTRUCTIONS** : QUESTION PAPERS MUST BE HANDED IN.

**REQUIREMENTS** : Use of scientific (non-programmable) calculator is permitted  
(only one per candidate).

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**INSTRUCTIONS TO CANDIDATES:**

- PLEASE ANSWER ALL THE QUESTIONS.
- Number each question clearly; the order of answer/s does not matter.
- Show all units in calculations.
- Write clearly and legibly

**Question One (Distillation)****[Total: 20 marks]**

As a chemical/ process engineer of TMI investments, a process engineering company in Africa, you are presented with the following situation. A tray distillation column is fed with a vapour at its dew point. The flow rates and compositions of the various streams associated with the distillation column are given in the table below:

Compound	Feed		Distillate		Bottoms		Relative volatility $\alpha$
	kmol	%	kmoles	%	Kmoles	%	
Benzene	60	60	48.5	93.0	11.5	24.1	2.4
toluene	30	30	3.6	7.0	36.4	55.0	1.0
xylene	10	10	0	0	10.0	20.9	0.45
Total	100	100	52.1	100	47.9	100	

Accordingly, advise management by way of answering the following questions:

- 1.1 Identify the light and heavy key components [2]
- 1.2 Identify the range of values of  $\theta$  that would be appropriate to use in the Underwood equation to find the minimum reflux ratio required for distillation (Hint: use 1.2 as the initial guess for  $\theta$ ) [6]
- 1.3 Use the Underwood equation to estimate the minimum reflux ratio [6]
- 1.4 Use the Fenske equation to estimate the minimum number of theoretical plates required for the distillation [6]

**Question Two (Crystallisation)****[Total: 20 Marks]**

2. A hot solution containing 1000 kg of MgSO<sub>4</sub> and water having a concentration of 30 wt% is cooled to 288.8 K, where crystals of MgSO<sub>4</sub>.7H<sub>2</sub>O are precipitated. The solubility at 288.8 K is 24.5 wt% anhydrous MgSO<sub>4</sub> in solution.

- 2.1 Derive an expression for the crystal yield,  $y$ , as a function of the concentration of anhydrous solute or salt,  $R$  (molecular mass of hydrate/molecular mass of anhydrous salt) and  $E$  (ratio mass of solvent evaporated/mass of solvent in the initial solution). [8]
- 2.2 Calculate the yield of crystals obtained if 10% of the original water evaporates on cooling. [12]

$$M [Mg] = 24.305 \text{ g/mol}; M [S] = 32.065 \text{ g/mol}; M [O] = 15.999 \text{ g/mol}; M [H] = 1.008 \text{ g/mol}$$

**Question Three (Evaporation)****[Total: 25 Marks]**

3. A sugar company ITM in KZN produces a juice concentrate at rate of  $4800 \text{ kg.hr}^{-1}$  in a single stage evaporator. The surface area for heat transfer is  $150 \text{ m}^2$  and the overall heat transfer coefficient is  $1800 \text{ W.m}^{-2}\text{K}^{-1}$ . Heat is supplied as saturated steam at a rate  $7075 \text{ kg.hr}^{-1}$  and pressure of  $150 \text{ kPa}$ . The vapour space pressure is maintained at pressure of  $65 \text{ kPa}$ . If the feed is supplied at  $25^\circ\text{C}$ ,

**Calculate:**

- 3.1 The boiling point rise for this unit [10]  
 3.2 The ratio of the mole fractions product and feed streams [15]

Given:  $C_p = 4000 \text{ J/kg/K}$

**Question Four (Fluidisation)****[Total: 25 Marks]**

- 4.1 Explain the effect of fluid velocity on pressure gradient. [5]  
 4.2 State any THREE (3) applications of fluidized bed solid techniques [3]  
 4.3 State any THREE (3) advantages of the fluidized beds for chemical reactions [3]  
 4.4 Spherical catalyst pellets  $4\text{mm}$  in diameter are to be fluidized with nitrogen at  $101.3\text{kPa}$  at  $60^\circ\text{C}$ . The density of the catalyst particles are  $960 \text{ kg/m}^3$ . The molecular weight of nitrogen is  $29\text{kg/kmol}$ . If it is assumed that the point of incipient fluidization is reached at  $e_{mf} = 0.430$   
 Calculate the minimum fluidization velocity in the vessel. [14]

Nitrogen is considered here to be an ideal gas with  $\mu_{nitrogen} = 0.0000207 \text{ Ns/m}^2$ .

**Question Five (Filtration)****[Total: 10 Marks]**

5. A plate and frame press gave a total of  $8 \text{ m}^3$  of filtrate in  $1800 \text{ s}$  and  $11.3 \text{ m}^3$  in  $3600 \text{ s}$  when filtration was stopped.

Estimate the washing time if  $3 \text{ m}^3$  of wash water is used. [10]

The resistance of the cloth may be neglected and a constant pressure is used throughout.

**END****[Total: 100 Marks]**

**Useful Formulae and Correlations**

Fenske's Equation(s):

$$N_{\min} + 1 = \frac{\log \left[ \left( \frac{x_{LK}}{x_{HK}} \right)_D \left( \frac{x_{HK}}{x_{LK}} \right)_B \right]}{\log \alpha_{LK,HK}}, \quad b_i = \frac{f_i}{1 + \left( d_r / b_r \right) (\alpha_{i,r})_m^{N_{\min}}}, \quad d_i = \frac{f_i \left( d_r / b_r \right) (\alpha_{i,r})_m^{N_{\min}}}{1 + \left( d_r / b_r \right) (\alpha, r)_m^{N_{\min}}}$$

Underwood's Equation(s):

$$\sum \frac{\alpha_i x_{iD}}{\alpha - \theta} = R_m + 1 \quad \alpha_{HK} < \theta < \alpha_{LK}$$

$$\sum \frac{\alpha_i x_{iF}}{\alpha - \theta} = 1 - q$$

Kirkbride's Equation(s):

$$\log \left[ \frac{N_r}{N_s} \right] = 0.026 \log \left[ \frac{W}{D} \left( \frac{x_{HK}}{x_{LK}} \right)_F \left( \frac{x_{LKW}}{x_{HKD}} \right)^2 \right], \quad \frac{N_r}{N_s} = \left[ \left( \frac{Z_{j,F}}{Z_{i,F}} \right) \left( \frac{x_{i,B}}{x_{j,D}} \right)^2 \left( \frac{B}{D} \right) \right]^{0.206}$$

Molokanov's Correlation:

$$\frac{N - N_{\min}}{N + 1} = 1 - \exp \left[ \left( \frac{1 + 54.4\Psi}{11 + 117.2\Psi} \right) \left( \frac{\psi - 1}{\psi^{0.5}} \right) \right] \text{ where: } \Psi \equiv \frac{R - R_{\min}}{R + 1}$$

Bubble and Dew point calculation(s):

$$\sum y_i = \sum K_i x_i = K_c \sum \alpha_i x_i = 1.0, \quad y_i = \frac{\alpha_i x_i}{\sum (\alpha_i x_i)}, \quad \sum_{i=1}^{N_c} y_i = \sum_{i=1}^{N_c} K_i x_i = 1.0, \quad (K_p) \text{Trial 2} = \frac{(K_p) \text{Trial 1}}{\sum K_i x_i},$$

$$\sum x_i = \sum \left( \frac{y_i}{K_i} \right) = \left( \frac{1}{K_c} \right) \sum \left( \frac{y_i}{\alpha_i} \right) = 0, \quad x_i = \frac{y_i / \alpha_i}{\sum (y_i / \alpha_i)}, \quad \sum_{i=1}^{N_c} x_i = \sum_{i=1}^{N_c} \frac{y_i}{K_i} = 1.0, \quad (K_i) \text{Trial 2} = (K_i) \text{Trial 1} \sum \frac{y_i}{K_i}$$

Erbar-Maddox correlation:

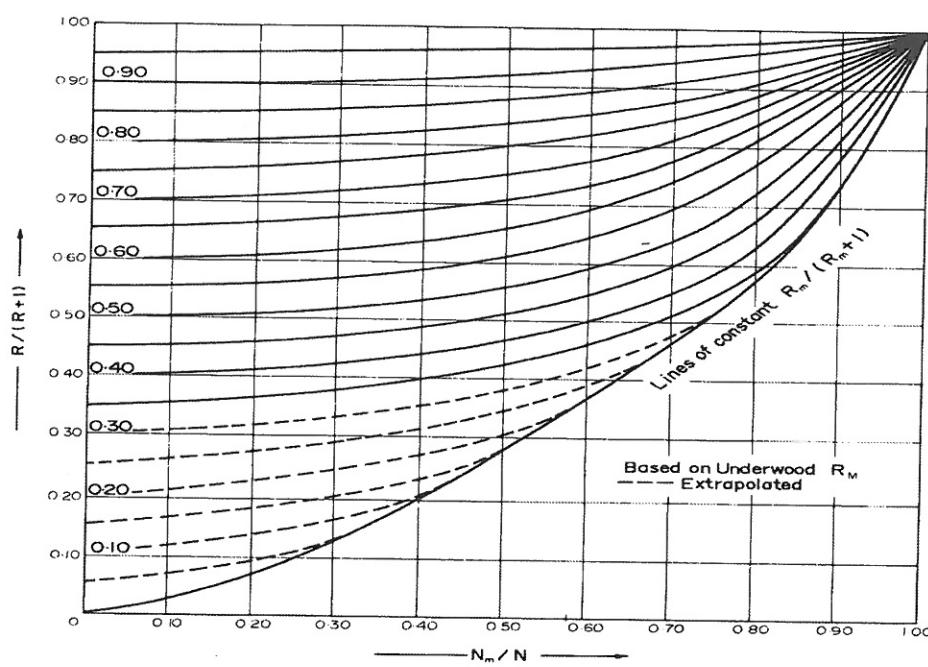
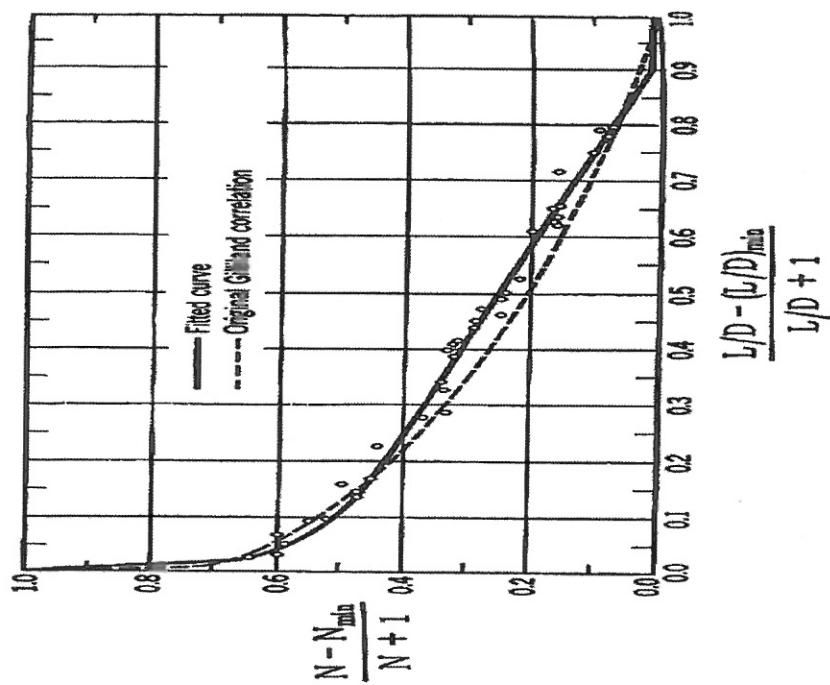
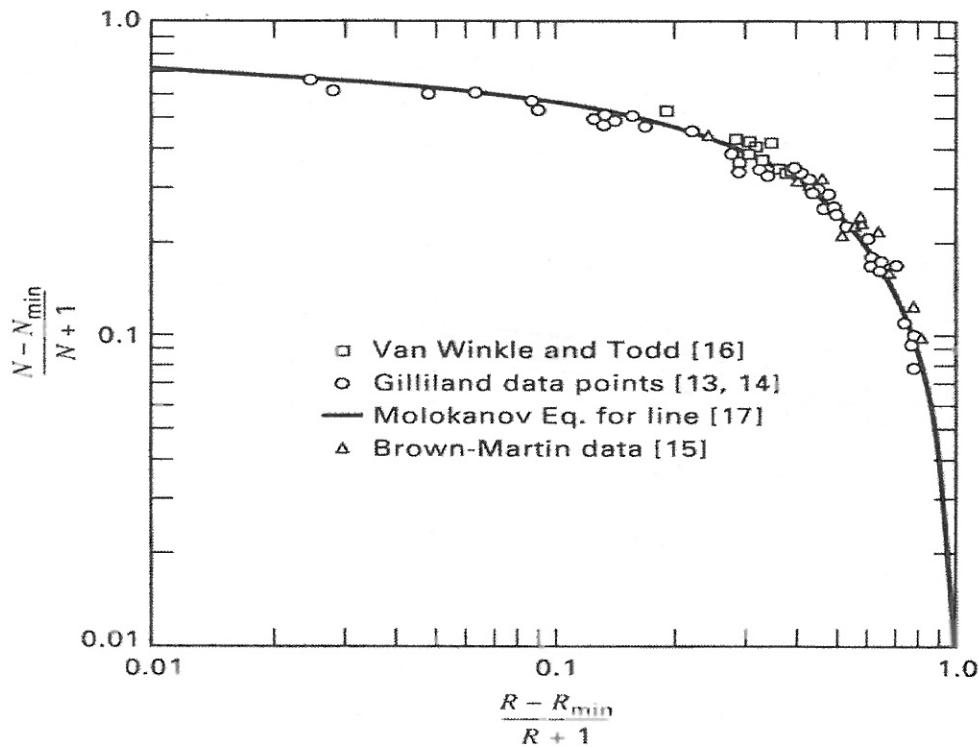


FIG. 11.11. Erbar-Maddox correlation (Erbar and Maddox, 1961)

$$\frac{R}{R+1} \text{ vs } \frac{N_m}{N} \quad \text{with} \quad \frac{R_m}{R_m+1} \quad \text{as a parameter}$$

Gilliland correlation:





Number of transfer units is given by:

$$N_{OG} = \int_{Y_1}^{Y_2} \frac{dY}{Y_e - Y} \quad \text{and} \quad N_{OL} = N_{OG} \left( \frac{mG_M}{L_M} \right)$$

Height of transfer unit is given by:

$$H_{OG} = \frac{G_M}{K_G a P}$$

Slope of q-line:  $-\left(\frac{f}{1-f}\right)$

$$f = \left( \frac{c_p(t_b - t_f)_{Liquid} + \Lambda_{Feed} + (c_p(t_b - t_f))_{saturated vapour}}{\Lambda} \right)$$

$$-\frac{\Delta P}{L} = \frac{150(1-\varepsilon)^2}{\varepsilon^3} \frac{\mu u_c}{d^2} + \frac{1.75(1-\varepsilon)}{\varepsilon^3} \frac{\rho u_c^2}{d}$$

$$(-\Delta P) = (1 - e_{mf}) (\rho_s - \rho) \lg$$

$$(1 - e_{mf})(\rho_s - \rho)g = \frac{150(1 - e_{mf})^2}{e_{mf}^3} \frac{\mu u_{mf}}{d^2} + \frac{1.75(1 - e_{mf})}{e_{mf}^3} \frac{\rho u^2}{d}$$

$$w_1 = w_2 + \left( y - \frac{y}{R} \right) + w_1 E$$

$$y = \frac{R w_1 [c_1 - c_2 (1 - E)]}{[1 - c_2 (R - 1)]}$$

$$\frac{1}{nF} \frac{V_w}{V_L} = \ln \frac{1 - F}{F}$$

$$P_a = P_a^o \left\{ \frac{n_a}{n_a + n_b + n_c + \dots} \right\} = x_a P_a^o$$

$$\Delta T = T_{steam} - T_b$$

$$\{m_{steam} x h_{fg}\} = \{m_{feed} C_p \Delta T\} + \{m_v x h_{fg}\} + \{m_L C_p \Delta T\}$$

$$Q = m_{steam} h_{fg} = m_{feed} C_p \Delta T + m_v h_{fg}$$

$$Q = m_{feed} C_p \Delta T + m_v h_{fg}$$

$$\frac{t - t_s}{V - V_s} = \frac{K_1(V + V_s)}{2P} + \frac{K_2}{P}$$

$$\theta_f = k_f \theta_c$$

$$\theta_f = \frac{K_1 V_f^2}{2P} + \frac{K_2 V_f}{P}$$

Table F.1 Saturated Steam, SI Units

$T$ K	$P$ kPa	SPECIFIC VOLUME $V$	INTERNAL ENERGY $U$				ENTHALPY $H$				ENTROPY $S$				
			sat. liq.	evap.	sat. liq.	evap.	sat. liq.	evap.	sat. liq.	evap.	sat. liq.	evap.	sat. liq.	evap.	
0.01	273.16	0.611	1.000	206300.	-0.04	2375.7	2375.6	-0.04	2501.7	2501.6	0.0000	9.1578	9.1578	0.0000	
1	273.16	0.611	1.000	206200.	0.00	2375.6	2375.6	0.00	2501.6	2501.6	0.0000	9.1575	9.1575	0.0000	
2	275.15	0.657	1.000	192600.	4.17	2372.7	2376.9	4.17	2499.2	2503.4	0.0153	9.1158	9.1158	0.0153	
3	276.15	0.705	1.000	179900.	8.39	2369.9	2378.3	8.39	2496.8	2505.2	0.0306	9.0741	9.0741	0.0306	
4	277.15	0.757	1.000	168200.	12.60	2367.1	2379.7	12.60	2494.5	2507.1	0.0459	9.0326	9.0326	0.0459	
5	278.15	0.813	1.000	157300.	15.80	2364.3	2381.1	16.80	2492.1	2508.9	0.0611	8.9915	8.9915	0.0611	
6	279.15	0.935	1.000	147200.	147200.	21.01	2361.4	2382.4	21.01	2489.7	2510.7	0.0762	8.9507	8.9507	0.0762
7	280.15	1.001	1.000	137800.	137800.	25.21	2358.6	2383.8	25.21	2487.4	2512.6	0.0913	8.9102	8.9102	0.0913
8	281.15	1.072	1.000	121000.	121000.	29.41	2355.8	2386.2	29.41	2485.0	2514.4	0.1063	8.8699	8.8699	0.1063
9	282.15	1.147	1.000	113400.	113400.	33.60	2353.0	2386.6	33.60	2482.8	2516.2	0.1213	8.8300	8.8300	0.1213
10	283.15	1.227	1.000	106400.	106400.	37.80	2350.1	2387.9	37.80	2480.3	2518.1	0.1362	8.7903	8.7903	0.1362
11	284.15	1.312	1.000	99910.	99910.	41.99	2347.3	2389.3	41.99	2477.9	2519.9	0.1510	8.7510	8.7510	0.1510
12	285.15	1.401	1.000	93630.	93630.	46.18	2344.5	2390.7	46.18	2475.5	2521.7	0.1658	8.7119	8.7119	0.1658
13	286.15	1.497	1.001	88180.	88180.	50.38	2341.7	2392.1	50.38	2473.2	2523.6	0.1805	8.6731	8.6731	0.1805
14	287.15	1.597	1.001	82900.	82900.	54.58	2338.9	2393.4	54.57	2470.8	2525.4	0.1952	8.6345	8.6345	0.1952
15	288.15	1.704	1.001	77980.	77980.	58.75	2335.1	2394.8	58.75	2468.5	2527.2	0.2098	8.5963	8.5963	0.2098
16	289.15	1.817	1.001	73380.	73380.	62.94	2332.2	2396.2	62.94	2466.1	2529.1	0.2243	8.5582	8.5582	0.2243
17	290.15	1.936	1.001	69390.	69390.	67.12	2330.4	2397.6	67.13	2463.8	2530.9	0.2388	8.5205	8.5205	0.2388
18	291.15	2.062	1.001	65090.	65090.	71.31	2327.6	2398.9	71.31	2461.4	2532.7	0.2533	8.4830	8.4830	0.2533
19	292.15	2.196	1.002	61340.	61340.	75.49	2324.8	2400.3	75.50	2459.0	2534.5	0.2677	8.4458	8.4458	0.2677
20	293.15	2.337	1.002	57840.	57840.	80.66	2319.2	2403.0	83.86	2457.3	2536.4	0.2820	8.4088	8.4088	0.2820
21	294.15	2.485	1.002	54560.	54560.	88.04	2316.4	2404.4	88.04	2452.0	2538.2	0.2963	8.3721	8.3721	0.2963
22	295.15	2.632	1.002	51490.	51490.	92.22	2313.6	2405.8	92.23	2449.6	2541.8	0.3105	8.3356	8.3356	0.3105
23	296.15	2.808	1.002	48620.	48620.	96.40	2310.7	2407.1	96.41	2447.2	2543.6	0.3247	8.2994	8.2994	0.3247
24	297.15	2.982	1.003	45930.	45930.	100.6	2307.9	2408.5	100.6	2444.9	2545.5	0.3389	8.2634	8.2634	0.3389
25	298.15	3.166	1.003	43400.	43400.	104.8	2305.1	2409.9	104.8	2442.5	2547.3	0.3530	8.2277	8.2277	0.3530
26	299.15	3.360	1.003	41030.	41030.	108.9	2302.3	2411.2	108.9	2440.2	2549.1	0.3670	8.1922	8.1922	0.3670
27	300.15	3.564	1.003	38810.	38810.	113.1	2299.5	2412.6	113.1	2437.8	2550.9	0.3810	8.1569	8.1569	0.3810
28	301.15	3.778	1.004	36730.	36730.	117.3	2293.7	2414.0	117.3	2435.4	2552.7	0.4088	8.1218	8.1218	0.4088
29	302.15	4.004	1.004	34770.	34770.	121.5	2293.8	2415.3	121.5	2433.1	2554.5	0.4227	8.0524	8.0524	0.4227



Table F.1 Saturated Steam, SI Units (Continued)

<i>t</i> °C	<i>P</i> kPa	SPECIFIC VOLUME <i>V</i>	INTERNAL ENERGY <i>U</i>	ENTHALPY <i>H</i>	ENTROPY <i>S</i>
		sat. liq.	sat. vap.	sat. liq.	sat. vap.
75	348.15	38.55	1.026	4133.1	313.9
76	349.15	40.19	1.027	3975.7	318.1
77	350.15	41.89	1.027	3823.3	315.2
78	351.15	43.65	1.028	3878.6	322.3
79	352.15	45.47	1.029	3540.3	326.5
80	353.15	47.36	1.029	3408.1	334.9
81	354.15	49.31	1.030	3281.6	339.1
82	355.15	51.33	1.031	3160.6	343.3
83	356.15	53.42	1.031	3044.8	347.5
84	357.15	55.57	1.032	2933.9	351.7
85	358.15	57.80	1.033	2827.8	355.9
86	359.15	60.11	1.033	2726.1	360.1
87	360.15	62.49	1.034	2628.8	364.3
88	361.15	64.95	1.035	2535.4	368.5
89	362.15	67.49	1.035	2446.0	372.7
90	363.15	70.11	1.036	2360.3	376.9
91	364.15	72.81	1.037	2278.0	381.1
92	365.15	75.61	1.038	2199.2	385.3
93	366.15	78.49	1.038	2123.5	392.5
94	367.15	81.46	1.039	2050.9	393.7
95	368.15	84.53	1.040	1981.2	397.9
96	369.15	87.69	1.041	1915.3	402.1
97	370.15	90.94	1.042	1850.0	405.3
98	371.15	94.30	1.042	1789.3	410.5
99	372.15	97.76	1.043	1729.0	414.7
100	373.15	101.33	1.044	1672.0	419.0
101	374.15	106.78	1.045	1564.5	427.4
102	375.15	116.68	1.047	1465.1	435.8
103	376.15	125.04	1.049	1373.1	444.3
104	377.15	133.90	1.050	1287.9	452.7
105	378.15	143.27	1.052	1208.9	461.2
106	379.15	153.16	1.054	1135.6	469.6
107	380.15	163.62	1.055	1067.5	478.1
108	381.15	174.65	1.057	1005.2	486.6
109	382.15	186.28	1.059	945.3	495.0
110	383.15	198.54	1.061	890.5	891.5
111	384.15	211.45	1.062	839.4	840.5
112	385.15	225.04	1.064	791.8	820.5
113	386.15	239.33	1.066	747.3	748.4
114	387.15	239.15	1.068	706.9	705.8
115	388.15	254.35	1.071		

sat.

liq.

evap.

vap.

*E.2. Steam Tables*

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130	270.13	667.1	2719.9	5.3917
132	286.70	1.070	596.9	7.0261
134	407.15	304.07	596.9	5.3944
136	409.15	322.29	1.074	5.3944
138	411.15	341.38	1.076	5.3944
140	413.15	361.38	1.080	5.3944
142	415.15	382.31	1.082	5.3944
144	417.15	404.20	1.084	5.3944
146	419.15	427.09	1.086	5.3944
148	421.15	451.01	1.089	5.3944
150	423.15	476.00	1.091	5.3944
152	425.15	502.08	1.093	5.3944
154	427.15	529.29	1.095	5.3944
156	429.15	557.67	1.098	5.3944
158	431.15	587.25	1.100	5.3944
160	433.15	618.06	1.102	5.3944
162	435.15	650.16	1.105	5.3944
164	437.15	683.56	1.107	5.3944
166	439.15	718.31	1.109	5.3944
168	441.15	754.45	1.112	5.3944
170	443.15	792.02	1.114	5.3944
172	445.15	831.06	1.117	5.3944
174	447.15	871.60	1.120	5.3944
176	449.15	913.68	1.122	5.3944
178	451.15	957.36	1.125	5.3944
180	453.15	1002.7	1.128	5.3944
182	455.15	1049.6	1.133	5.3944
184	459.15	1098.3	1.136	5.3944
186	461.15	1148.8	1.139	5.3944
188	463.15	1201.0	1.139	5.3944
190	465.15	1255.1	1.142	5.3944
192	465.15	1311.1	1.144	5.3944
194	467.15	1369.0	1.147	5.3944
196	469.15	1428.9	1.150	5.3944
198	471.15	1490.9	1.153	5.3944
200	473.15	1554.9	1.156	5.3944
202	475.15	1621.0	1.160	5.3944
204	477.15	1689.3	1.163	5.3944
206	479.15	1759.8	1.166	5.3944
208	481.15	1832.6	1.169	5.3944
210	483.15	1907.7	1.173	5.3944
212	485.15	1985.2	1.176	5.3944
214	487.15	2065.1	1.179	5.3944
216	489.15	2147.5	1.183	5.3944
218	491.15	2232.4	1.186	5.3944

Table F.1 Saturated Steam, SI Units (Continued)

$t$ $^{\circ}$ C	P kPa	T K	SPECIFIC VOLUME V sat. liq.	INTERNAL ENERGY U sat. vap.	ENTHALPY H sat. liq.	ENTROPY S sat. liq.
220	493.15	2319.8	1.190	84.85	86.04	940.9
220	495.15	2409.7	1.194	82.86	950.1	950.7
224	497.15	2502.7	1.201	79.82	952.9	952.9
224	499.15	2582.2	1.205	75.71	969.4	969.4
228	501.15	2686.5	1.205	72.92	977.6	971.5
228	503.15	2797.6	1.209	70.24	974.12	980.18
230	503.15	2901.6	1.213	67.68	986.9	989.3
232	505.15	3068.6	1.217	65.22	996.2	999.7
234	507.15	3118.6	1.221	62.86	1004.8	1005.4
236	509.15	3231.7	1.225	60.80	1024.1	1024.1
238	511.15	3347.8	1.229	58.43	1035.5	1035.5
240	513.15	3457.2	1.233	56.34	1042.9	1042.9
242	515.15	3569.8	1.238	54.34	1052.3	1052.3
244	517.15	3715.7	1.242	52.41	1061.8	1061.8
246	519.15	3844.9	1.247	50.56	1071.3	1071.3
248	521.15	3977.6	1.251	48.79	1080.8	1080.8
250	523.15	4113.7	1.256	47.08	1090.4	1090.4
252	525.15	4253.4	1.261	45.43	1100.0	1100.0
254	527.15	4396.7	1.266	43.85	1109.6	1109.6
256	529.15	4543.7	1.271	42.33	1119.3	1119.3
258	531.15	4694.3	1.276	40.86	1129.7	1129.7
260	533.15	4846.8	1.281	39.44	1138.7	1138.7
262	535.15	5007.1	1.286	37.87	1149.5	1149.5
264	537.15	5169.3	1.281	36.77	1160.3	1160.3
266	539.15	5335.6	1.297	35.51	1178.2	1178.2
268	541.15	5505.8	1.303	34.29	35.59	1187.1
270	543.15	5680.8	1.308	33.11	34.42	1195.9
272	545.15	5859.7	1.314	31.97	33.29	1204.7
274	547.15	6041.5	1.320	30.88	32.20	1208.0
276	549.15	6222.7	1.326	29.82	31.14	1218.1
278	551.15	6424.2	1.332	29.79	30.13	1228.3
280	553.15	6647.2	1.332	29.79	30.13	1236.7
282	555.15	6861.6	1.336	29.74	30.11	1246.5
284	557.15	7021.8	1.345	28.85	28.20	1258.7
286	559.15	7231.5	1.352	26.93	26.72	1268.0
288	561.15	7446.1	1.366	25.54	26.39	1279.4
290	563.15	7665.4	1.373	24.17	25.54	1287.7
292	565.15	7887.7	1.381	23.33	25.71	1297.5
294	567.15	8118.9	1.388	22.52	25.80	1300.9
296	569.15	8353.2	1.396	21.74	23.13	1311.8
298	571.15			20.98	22.38	1322.2

